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POLYMERIC BINDERS HAVING SPECIFIC PEEL AND CURE PROPERTIES AND USEFUL IN MAKING CREPED WEBS

BACKGROUND OF THE INVENTION

[0001] Crepe processes, especially double recrepe (DRC) processes, have been used to produce paper products, such as paper towels and wipes, with specific properties.

The DRC process involves creping a base sheet or nonwoven web on a drum, printing a polymeric binder on one side of the sheet, flash drying the binder, creping the base sheet on a drum again, printing a polymeric binder on the other side of the base sheet, flash drying the binder, and then creping the base sheet a third time. The base sheet is printed while traveling through gravure nip rolls. Various crepe processes and binding materials used in the processes are known. Examples of such processes are disclosed in U.S. 3,879,257, U.S. 3,903,342, U.S. 4,057,669, U.S. 5,674,590, and U.S. 5,776,306.

[0002] In order for the base sheet or web to adhere adequately to the creping drum, polymeric binders used in creping processes are typically emulsion polymers containing surfactants that are based on alkylphenol ethoxylates (APEs). Known emulsion polymeric binders, that are free of alkylphenol ethoxylates, have not been effective in creping processes, especially DRC processes, because they do not provide the necessary adhesion to creping drums, produce an unacceptable amount of foam, are too low in viscosity, decompose at elevated temperatures, causing an unacceptable odor, and/or are subject to felt filling.

[0003] Appropriate binders for making paper products using a crepe process should be free of APE-based surfactants, adhere to a creping drum, provide a high degree of softness and absorbency to the finished product, and not felt-fill.

[0004] Heretofore, specific measurable properties for predicting the effectiveness of binders for a crepe process have not been reported.

BRIEF SUMMARY OF THE INVENTION

- 5 **[0005]** This invention is directed to APE-free polymer binders formed by emulsion polymerization techniques and having a specific peel value and a specific cure profile. Binders having the peel value and cure profile described herein can be considered for use in crepe processes, especially DRC processes. According to this invention, the APE-free polymeric binders have a peel value, when adhered to a heated metal surface, of 35% to 200% of the peel value shown by a standard APE-based polymer binder control (i.e., AIRFLEX® 105 vinyl acetate-ethylene (VAE) polymer emulsion) and exhibit a cure profile such that at least 55 % cure is achieved within 30 seconds at a temperature required for cure. Wet tensile strength is used to determine the cure profile. The peel value is determined by a modified release and adhesion test.
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- 15 **[0006]** Binders having the properties described above are excellent candidates for use in crepe, especially DRC, processes. When used in making paper products, they should adhere to the creping drum providing a high degree of softness and absorbency to the finished paper product and not felt-fill; thus reducing production breaks, while ensuring that the desired finished product is manufactured.

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DETAILED DESCRIPTION OF THE INVENTION

- [0007]** Any APE-free polymer prepared according to well known emulsion polymerization techniques and manifesting the requisite cure profile and peel value is suitable in this invention.
- 25 **[0008]** APE-free polymer emulsions can be formed by polymerizing one or more ethylenically unsaturated monomers and optionally one or more crosslinking monomers,

under emulsion polymerization conditions, in the presence of a combination of a specific anionic surfactant and a specific nonionic surfactant, wherein said anionic surfactant is a sodium laureth sulfate having 1 to 12 moles of ethylene oxide, said nonionic surfactant is a secondary alcohol ethoxylate containing 7 to 30 moles of ethylene oxide or an
5 ethoxylated branched primary alcohol containing 3 to 30 moles of ethylene oxide, said primary or secondary alcohol containing 7 to 18 carbons

[0009] Ethylenically unsaturated monomers that can be used in the preparation of the polymer emulsions of this invention include, but are not limited to, vinyl esters, such as vinyl acetate, ethylene, styrene, butadiene, C₁₋₈ alkyl esters of acrylic and methacrylic
10 acid, such as methyl (meth)acrylate, ethyl (meth)acrylate, butyl (meth)acrylate, hexyl (meth)acrylate, 2-ethylhexyl (meth)acrylate, diacrylates, unsaturated carboxylic acid, such as acrylic, methacrylic, crotonic, itaconic, and maleic acid, acrylonitrile, and vinyl esters of C₂₋₁₀ alcohols.

[0010] The polymer can contain up to 10 % of one or more crosslinking monomers.

15 Examples of crosslinking monomers are N-(C₁₋₄) alkylol (meth)acrylamide, such as N-methylol acrylamide, *i*-butoxy methylacrylamide, acrylamidoglycolic acid, acrylamidobutyraldehyde, and the dialkyl acetal of acrylamidobutyraldehyde in which the alkyl can have 1 to 4 carbons. Any of the crosslinking monomers can be used alone, together, or in combination with acrylamide.

20 **[0011]** Polymer emulsions comprising 50 to 90 wt % (preferably 70 to 85 wt %) vinyl acetate, 5 to 44 wt % (preferably 10 to 30 wt %) ethylene, and 1 to 10 wt % (preferably 3 to 8 wt %) one or more crosslinking monomer, based on the total weight of monomers, can be formed using the surfactant package described herein.

[0012] The emulsion polymerization may be conducted in a stage or sequential manner
25 and can be initiated by thermal initiators or by a redox system. A thermal initiator is

typically used at temperatures at or above about 70 °C and redox systems are preferred at temperatures below about 70 °C. The amount of thermal initiator used in the process is 0.1 to 3 wt %, preferably more than about 0.5 wt %, based on total monomers.

Thermal initiators are well known in the emulsion polymer art and include, for example, ammonium persulfate, sodium persulfate, and the like. The amount of oxidizing and reducing agent in the redox system is about 0.1 to 3 wt %. Any suitable redox system known in the art can be used; for example, the reducing agent can be a bisulfite, a sulfoxylate, ascorbic acid, erythorbic acid, and the like. Examples of oxidizing agent are hydrogen peroxide, organic peroxides, such as *t*-butyl peroxide or *t*-butyl hydroperoxide, persulfates, and the like.

[0013] Effective emulsion polymerization reaction temperatures range from about 50 and 100 °C; preferably, 75 to 90 °C, depending on whether the initiator is a thermal or redox system.

[0014] The specific combination of anionic and nonionic surfactants for the emulsion polymerization process has been shown to produce crosslinking polymer emulsions that are effective as binders in a creping process, especially a DRC process. The anionic surfactant is a sodium laureth sulfate having 1 to 12, preferably 2 to 5, moles of ethylene oxide. An example of an appropriate anionic surfactant is Disponil FES 32 IS (sodium laureth sulfate containing 4 moles of ethylene oxide), supplied by Cognis as a 30 % aqueous solution. The nonionic surfactant is a secondary alcohol ethoxylate, such as 2-pentadecanol ethoxylate, containing 7 to 30 moles, preferably 12 to 20 moles, of ethylene oxide or an ethoxylated branched primary alcohol, such as tridecanol ethoxylate, containing 3 to 30 moles, preferably 9 to 20 moles, of ethylene oxide. The primary or secondary alcohol can contain 7 to 18, preferably 9 to 14 carbons. An example of an appropriate nonionic surfactant is Tergitol 15-S-20 (a secondary alcohol

ethoxylate containing 20 moles of ethylene oxide), supplied by Dow as an 80 % aqueous solution.

5 **[0015]** The amount of active surfactant, based on total polymer, can be 1 to 5 wt % (preferably 1.5 to 2 wt %) for the anionic surfactant and 0.25 to 5 wt % (preferably 0.5 to 1.5 %) for the nonionic surfactant. The weight ratio of anionic to nonionic surfactant can range from 4:1 to 1.5:1. A weight ratio of 65:35 (anionic:nonionic surfactant) has been found to give a latex that provides appropriate adhesion to creping drums, has a moderate viscosity with little foam generation, results in less off-gassing than APE-based latexes, and has an accelerated sedimentation of no greater than 1 %.

10 **[0016]** The peel value of prospective polymeric binders for use in crepe processes, especially DRC processes can be measured using the following adhesion and release procedure:

15 **[0017]** A 2-inch x 6-inch x 1/32-inch stainless steel plate was attached to a movable heated (350 °F; 177 °C) inclined (45°) metal platform and allowed to equilibrate to the temperature of the platform (2 minutes.) Approximately 0.42 g of the polymer emulsion is applied to a 1½-inch x 6-inch piece of bleached, mercerized cotton poplin. The jaws of a Testing Machine, Inc. gram tensile measuring apparatus are attached to one of the long ends of the cotton poplin. The coated side of the coated cotton poplin is then pressed onto the heated stainless steel plate with a 3-pound lab roller by rolling the lab roller back and forth over the substrate for 10 seconds. After 30 seconds, the stainless steel plate is moved away from the tensile measuring device (to which the substrate is attached) at a rate of 12 inches/minute (30.48 cm/minute). The amount of force needed to remove the cotton from the stainless steel plate is recorded and compared to AIRFLEX 105 VAE emulsion control.

25 **[0018]** The AIRFLEX 105 polymer emulsion can be prepared in small batches as follows: Initially charge a one-gallon, stirred, stainless steel reaction vessel with 883.5 g

of deionized water, 305 g of Polystep OP-3S surfactant mixture (20 % active) of octylphenol ethoxylate (3 moles) and sodium sulfate salt of octylphenol ethoxylate (3 moles), supplied by Stefan, 0.91 g of sodium citrate, 3.5 g of 50 % aqueous citric acid, 2.3 g of 5 % aqueous ferric ammonium sulfate, and 312.0 g of vinyl acetate. While stirring, introduce 240.0 g of ethylene below the surface of the liquid in the reaction vessel in order that the interpolymers have a vinyl acetate:ethylene ratio of about 80:20. Heat the reaction vessel to 50 °C. Upon equilibration, add the following four aqueous solutions intermittently to the reaction vessel over the course of the reaction (on a delay basis); 15 % sodium formaldehyde sulfoxylate (SFS), 3.0 % *t*-butylhydroperoxide (*t*-bhp), 1246.0 g of vinyl acetate and 324.0 g of a 30% aqueous solution of N-methylol acrylamide (NMA). After three hours, terminate the vinyl acetate delay. Complete the NMA delay after four hours, and continue the other two delays for another 30 minutes. Terminate the reaction by cooling.

[0019] The cure profile is determined by measuring wet tensile strength. The following procedure can be followed:

[0020] A 2-inch x 6-inch unbonded DRC basesheet at about 65 gsm basis is coated with a binder and the binder is cured at 320 °F (160 °C) for 30 seconds and for 180 seconds. The cup of a Finch Wet Strength apparatus from Thwing-Albert, Philadelphia, is filled with an aqueous solution containing approximately 1 % active Aerosol OT-75 wetting surfactant (from Cytex Industries). The cured coated basesheet is then placed around the bar on the Finch cup attachment and the two long ends of the sample are clamped to the top jaw. The Finch cup holder is pulled over the middle of the coated basesheet and the coated basesheet is allowed to soak in the aqueous surfactant solution for 15 seconds. The coated basesheet is then pulled away from the bar until the basesheet breaks. The force required to break the basesheet is recorded. If the wet tensile strength of the bound basesheet cured for 30 seconds is at least 75 % the wet

strength of the 180-second cured bound basesheet, the binder will not felt-fill due to insufficient cure. For purposes of evaluating binders for use in a crepe process, at least 55 %, of the ultimate wet tensile strength is achieved within 30 seconds at the cure temperature.

5 **[0021]** Polymer binders that show a peel value of 35 % to 200 % (preferably 50 % to 125 %) of AIRFLEX 105 VAE emulsion control and a cure profile in which at least 55 % of the ultimate wet strength is achieved in 30 seconds at the cure temperature, are considered important candidates as binders for a crepe process, especially a DRC process.

10 **[0022]** To be used in a crepe process, especially a DRC process, the polymer emulsions identified by the peel and cure tests described above, should have a viscosity of 5 to 80 cps at about 30 % solids, and should be capable of being thickened to 100 cps with a thickener, such as a hydroxyethyl cellulose-based thickener. Viscosity is measured using a Brookfield viscometer, Model LVT, spindle #3 at 60 rpm. The
15 emulsion polymers of this invention should also be stable at temperatures up to about 550 °F (288 °C). The polymer emulsions should produce a minimal amount of foam when pumped and beaten during a DRC process.

20 **[0023]** Binders identified by this invention can be used in crepe processes well known in the art. Examples of crepe processes are described in the publications listed in the "Background of the Invention" section of the specification. Nonwoven webs typically used in a crepe process are wood pulp (alone or blended with natural or synthetic fibers) processed by a dry (air-laid, carded, rando) or wet-laid process.

25 **[0024]** The amount of binder applied to the web can vary over a wide range; for example, about 5 to 40 %; preferably 10 to 35 % of the finished product. When the products are wiper products, it is desirable to keep the amount to a minimum.

[0025] The invention will be further clarified by a consideration of the following examples, which are intended to be purely exemplary of the use of the invention.

EXAMPLE

- 5 **[0026]** Emulsion polymerization of vinyl acetate, ethylene, and N-methylol acrylamide was carried out in presence of various surfactant systems in a one-gallon stirred, stainless steel reaction vessel equipped with a jacket. In Run 1, reaction vessel was charged initially with 883.5 g of deionized water, 126.75 g of Disponil FES 32 IS, 25.625 g of Tergitol 15-S-20, 0.91 g of sodium citrate, 3.5 g of 50 % aqueous citric acid, 10 2.3 g of 5 % aqueous ferric ammonium sulfate and 312.0 g of vinyl acetate. While stirring, 240.0 g of ethylene was introduced below the surface of the liquid in the reaction vessel in order that the interpolymers would have a vinyl acetate:ethylene ratio of about 80:20. The reaction vessel was heated to 50 °C. Upon equilibration, the following four aqueous solutions were intermittently added to the reaction vessel over the course of the 15 reaction (on a delay basis); 15% sodium formaldehyde sulfoxylate (SFS), 3.0 % *t*-butylhydroperoxide (*t*-bhp), 1246.0 g of vinyl acetate and 324.0 g of a 30% aqueous solution of N-methylol acrylamide (NMA). After three hours, the vinyl acetate delay was terminated. After four hours the NMA delay was complete and the other two delays continued for another 30 minutes. The reaction was terminated by cooling.
- 20 **[0027]** Using the same emulsion recipe as Run 1, several surfactant packages were examined. The viscosity, emulsion stability, accelerated sedimentation, peel (% of AIRFLEX 105 VAE emulsion control), and 30-second wet tensile strength (% of ultimate wet tensile strength) were measured.
- [0028]** Viscosity was measured using a Brookfield viscometer, Model LVT, spindle #3 25 @ 60 rpm and 77 °F (25 °C), at about 24 hours after preparation to allow for cooling and the finishing of any residual-free monomer.

[0029] Emulsion stability was measured by measuring the viscosity at 4 intervals: after forming the polymer emulsion; after 3 days in a 120 °F oven; after 1 week in a 120 °F oven; and after 2 weeks in a 120 °F oven.

5 **[0030]** Accelerated sedimentation was measured by taking a sample of product and diluting it in half with water, spinning it in a centrifuge for five minutes at a predetermined setting, e.g., 2800 rpm \pm 100, and measuring the amount of precipitate forced to the bottom of the tube. When a one-gallon reactor is used, an accelerated sedimentation higher than 1 % is considered unsatisfactory. However in a plant-size operation, up to about 3 % is acceptable.

10 **[0031]** The peel value and the wet tensile strength of each of the binders were determined as described above.

[0032] The results of the tests are presented in the table below:

TABLE

Run	Anionic surfactant	Nonionic surfactant	Ratio of Anionic to Nonionic	% Solids	Viscosity, cps	Accelerated Sedimentation, %	Peel Value (% control)	30-second wet tensile (% of ultimate)
1	Disponil FES 32 IS	Tergitol 15-S-20	1.86	52.9	660	1.0	100	79.4
2	B-330S	Tergitol 15-S-20	1.86	53.2	532	4.0	47	70.0
3	Rhodapex ES	Tergitol 15-S-20	1.86	53.2	632	2.5	73	no data
4	FES 993	Tergitol 15-S-20	1.86	53.1	160	8.0	57	60.9
5	Steol 4N	Tergitol 15-S-20	1.86	53.1	348	2.0	48	66.6
6	Texapon NSO	Tergitol 15-S-20	1.86	53.2	152	6.0	75	92.9
7	Disponil FES 32 IS	Disponil 3065	1.86	53.3	600	3.0	175	78.4
8	Disponil FES 32 IS	Disponil 1080	1.86	53.3	490	4.0	200	72.6
9	Disponil FES 32 IS	TD-3	1.86	53.0	318	2.0	110	no data
10	DOSS	Tergitol 15-S-20	1.86	57.0	86	1.0	135	47.3
11	DOSS	Tergitol 15-S-20	1	53.4	372	0.5	100	34.2
12	DOSS	Tergitol 15-S-20	3	53.1	54	1.0	35	35.7
13	DOSS	Tergitol 15-S-20	0.33	53.3	116	0.5	130	43.7
14	DOSS	Tergitol 15-S-20	0.67	60.3	474	1.5	105	84.8
15	Tergitol 15-S-3 sulfate	Tergitol 15-S-20	2	55.8	600	10	68	72.1
16	DOSS	Tergitol 15-S-3	0.67	60.5	228	3.5	90	61.4
17	EST-30	Makon TD-3	2	54.2	810	1.5	67	78.7

Disponil FES 32 IS = sodium laureth sulfate containing 4 moles of ethylene oxide, supplied by Cognis
Tergitol 15-S-20 = a secondary alcohol ethoxylate containing 20 moles of ethylene oxide, supplied by Dow

5 B-330S = sodium laureth sulfate (3 moles) supplied by Stepan
Rhodapex ES = sodium laureth sulfate (3 moles) supplied by Rhodia
FES 993 = sodium laureth sulfate (1 mole) supplied by Cognis
Steol 4N = sodium laureth sulfate (4 moles) supplied by Stepan
Texacon NSO = sodium laureth sulfate (2 moles) supplied by Cognis
DOSS = dioctyl sulfosuccinate
10 Tergitol 15-S-3 Sulfate = secondary alcohol ethoxylate sulfate (3 moles) supplied by Dow
EST-30 = sodium trideceth sulfate (3 moles) supplied by Rhodia
Disponil 3065 = lauryl alcohol ethoxylate (30 moles) supplied by Cognis
Disponil 1080 = lauryl alcohol ethoxylate (10 moles) supplied by Cognis
Makon TD-3 = tridecyl alcohol ethoxylate (3 moles) supplied by Stepan

15 [0033] The peel value and wet tensile data show that the binders of Runs 1-2, 4-8, and 14-17 can be considered for use as binders in crepe processes, especially DRC processes. The binders of Runs 10-13 would be inappropriate for consideration as potential binders in crepe processes because the 30-second wet tensile strength is less
20 than 55 % of the ultimate wet tensile strength of the binder. Without cure data, Runs 3 and 9 are questionable for use in a crepe process.